Listing of Claims:

- 1. (Original) A homogeneous process for the hydrogenation of dicarboxylic acids and/or anhydrides in the presence of a catalyst comprising:
 - (a) ruthenium, rhodium, iron, osmium or palladium; and
 - (b) an organic phosphine;

wherein the hydrogenation is carried out in the presence of at least about 1% by weight water and wherein the reaction is carried out at a pressure of from about 500 psig to about 2000 psig and a temperature of from about 200 °C to about 300 °C such that from about 1 mol to about 10 mol of hydrogen are used to strip 1 mole of product from the reactor.

- 2. (Original) A process according to Claim 1 wherein the process is a continuous process comprising the steps of:
- (a) feeding the dicarboxylic acid and/or anhydride to the hydrogenation reactor;
 - (b) hydrogenating the dicarboxylic acid and/or anhydride;
 - (c) recovering the product in an hydrogen stream;
 - (d) separating the product from the hydrogen stream;
 - (e) recycling the hydrogen stream to the reactor;
- (f) separating any removed catalyst and recycling the catalyst to the reactor; and
 - (g) recovering the product.
- 3. (Currently Amended) A process according to Claim 1 [[or 2]] wherein the dicarboxylic acid and/or anhydride is a C_4 dicarboxylic acid or anhydride such that the process is a process for the production of butanediol, tetrahydrofuran and/or γ -butyrolactone.

- 4. (Original) A process according to Claim 3 wherein any γ -butyrolactone produced in the hydrogenation reaction is recycled to the hydrogenation reactor.
- 5. (Currently Amended) A process according to Claim 3 [[or 4]] wherein the C₄ dicarboxylic acid or anhydride is fumaric acid, maleic anhydride, maleic acid, succinic acid or succinic anhydride.
- 6. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 5]] wherein the water is present as the solvent for the reaction.
- 7. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 5]] wherein one or both of the reactants or the product are the solvent for the catalyst.
- 8. (Original) A process according to Claim 7 wherein a solvent is used and the water is present as an additive in the solvent.
- 9. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 5]] wherein the water is produced in situ as a by-product of the hydrogenation reaction.
- 10. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 9]] wherein the reaction takes place in more than one reactor and the reactors are operated in series.
 - 11. (Currently Amended) A process according to any one of

Claim[[s]] 1 [[to 9]] wherein the reaction is carried out at a pressure of about 900 psig.

- 12. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 10]] wherein the reaction is carried out at a temperature of about 240 °C to about 250 °C.
- 13. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 12]] wherein the catalyst is a ruthenium/phosphine catalyst.
- 14. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 13]] wherein, the ruthenium is present in an amount of from 0.0001 to 5 mol as ruthenium per liter of reaction solution.
- 15. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 14]] wherein the phosphine is tridentate phosphine.
- 16. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 14]] wherein the phosphine is selected from trialkylphosphines, dialkylphosphines, monoalkylphosphines, triarylphosphines, diarylphosphine, monoarylphosphines, diarylmonoalkyl phosphines and dialkylmonoaryl phosphines.
- 17. (Currently Amended) A process according to Claim 16 wherein the phosphine is selected from tris-1,1,1- (diphenylphosphinomethyl) methane, tris-1,1,1- (diphenylphosphinomethyl) -ethane, tris-1,1,1- (diphenylphosphinomethyl) propane, tris-1,1,1-

(diphenylphosphinomethyl) butane, tris-1,1,1(diphenylphosphinomethyl) 2,2dimethylpropane, tris-1,3,5(diphenylphosphinomethyl) cyclohexane, tris-1,1,1(dicyclohexylphosphinomethyl) ethane, tris-1,1,1(dimethylphosphinomethyl) ethane, tris1,1,1(diethylphosphinomethyl) ethane, 1,5,9-triethyl-1,5-9triphosphacyclododecane, 1,5,9-triphenyl-1,5-9triphosphacyclododecane, bis(2-diphylephosphinoethyl)
phenylphosphine, bis-1,2-(diphenyl phosphino) ethane, bis-1,3(diphenyl phosphino) propane, bis-1,4-(diphenyl phosphino) butane,
bis-1,2-(dimethyl phosphino) ethane, bis-1,3-(diethyl
phosphino) propane, bis-1,4-(dicyclohyxyl phosphino) butane,
tricyclohexylphosphine, trioctyl phosphine, trimethyl phosphine,
tripyridyl phosphine, and triphenylphosphine.

- 18. (Original) A process according to Claim 16 wherein the phosphine is selected from tris-1,1,1- (diarylphosphinomethyl)alkane and tris-1,1,1- (dialkylphosphinomethyl)alkane.
- 19. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 18]] wherein, the phosphine is present in in an amount of from 0.0001 to 5 mol as phosphine per liter of reaction solution.
- 20. (Currently Amended) A process according to any one of Claim[[s]] 1 [[to 19]] wherein the catalyst is regenerated in the presence of water and hydrogen.